PATENT SPECIFICATION

1 569 611 (11)

(21) Application Nos. 2606/76 (22) Filed 23 Jan. 1976

(61) Patent of Addition to No. 1520247 Dated 24 Jul. 1975

(23) Complete Specification Filed 13 Jan. 1977

(44) Complete Specification Published 18 Jun. 1980

(51) INT. CL. ³ A61K 9/72

(52) Index at Acceptance A5B 832 X



(54) PELLETISED OR GRANULAR MEDICAMENT FORMULATION

(71) We, FISONS LIMITED, a British Company of Fison House, 9 Grosvenor Street, London W1X OAH, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:

The present invention relates to a pharmaceutical composition and its preparation. In our British Patent No. 1,122,284 we have described and claimed an insufflator device for use in the administration of powdered medicaments by inhalation comprising a propeller-like device carrying a powder capsule rotatably mounted within a tubular housing by means of a shaft loosely journalled in a tapered bearing tube, the housing having a mouthpiece whereby a user can inhale air through the device. With that device, and other devices, e.g. that described in British Patent Specification No. 1,331,216, a user inhales air through the device which causes a powder container mounted therein to rotate. Powder within the container is fluidised and dispensed into the air stream which is inhaled by the user. For optimum dispensing it has been found that the powdered medicament particles should be comparatively free-flowing and yet should have an ultimate particle size of less than about ten microns to ensure adequate penetration of the medicament into the lungs of the user. These two requirements are prima facie mutually exclusive, since such fine powders are not sufficiently free-flowing. We have now found that this problem can be mitigated or overcome by forming the powdered medicament into small soft pellets or granules which will fluidise satisfactorily within the container and yet which are of sufficiently low internal coherence to break up into finer particles of medicament of a therapeutically effective size in the turbulent airstream around the outside of the container. The formation of the medicament into soft pellets or granules also aids the filling of the medicament into capsules and can enable diluents such as coarse lactose, which have in the past been incorporated into powder inhalation compositions, to be omitted from the

composition. Accordingly, the present invention provides a medicament in pellet or granule form, wherein the pellet or granule is soft, is from 10 to 1,000, preferably 30 to 500, microns in diameter and comprises an agglomeration of individual medicament particles, at least 90% and preferably at least 95% by weight of which have a diameter of less than 10 microns,

characterised in that the pellets or granules have
(i) a Total Transmitted Load Reduction (as hereinafter defined) of greater than 100, preferably greater than 400, more preferably greater than 800 and most preferably greater than 1,000 gms, and/or

(ii) a product of 'Total Transmitted Load Reduction' (as hereinafter defined) and 'Response Lag' (as hereinafter defined) of greater than 30, preferably greater than 40, and

more preferably between 40 and 1,000 g/cms, and/or (iii) a 'Response Lag' (as hereinafter defined) of at least 0.3, preferably of at least 0.4, and more preferably of between 0.4 and 0.8 cms.

The soft pellet or granule preferably has an internal coherence such that the pellet or granule remains intact when filled into a container, e.g. a capsule, using automatic or semi-automatic filling machines, under conditions of transport and storage, and when fluidised within a container in the device from which it is intended to dispense the pellets or granules and yet may be broken up into particles of a therapeutically effective size outside the container as it discharges from the container.

5

10

15

20

25

30

35

45

The medicament in the soft pellets or granules of the invention may be selected from a wide range of powdered medicaments and may be in amorphous or crystalline form and may have been comminuted, e.g. ground, and, if necessary, classified or sieved, e.g. on an air jet sieve, to obtain a suitable size or may have been made by direct crystallisation to the desired size. However, it is preferred that the medicament be one which is to be administered by inhalation and which has particles at least 90% of which, e.g. greater than 95% by weight of which, are of less than 10 microns, e.g. from 0.01 to 10, and preferably from 1 to 4, microns diameter, before incorporation into the soft pellets of the invention. Desirably the individual medicament particles are self-agglomerative as is usually the case with a hygroscopic material. Examples of suitable medicaments include those suitable for the inhalation treatment of allergic airway diseases such as pharmaceutically acceptable salts of 1,3-bis(2-carboxychromon-5-yloxy)propan-2-ol, pharmaceutically acceptable salts of 1,3-bis(2-carboxychromon-7-yloxy)propan-2-ol, sympathomimetic amines (e.g. isoprenaline, ephedrine, or isoetharine and salts thereof), antibiotics (e.g. tetracy-15 cline), steroids, enzymes, vitamins and antihistamines. If desired a mixture of medicaments, e.g. a mixture of the disodium salt of 1.3-bis(2-carboxychromon-5-yloxy)propan-2-ol (commonly known as sodium cromoglycate, disodium cromoglycate or cromolyn sodium) and isoprenaline, may be used. The pellets or granules may contain other ingredients, e.g. diluents colouring and flavouring agents. Where the medicament is not self agglomerative, e.g. hygroscopic, it may be desirable to incorporate a small portion of a binder into the soft pellets or granules. Suitable binders include acacia gum, tragacanth gum, celluloses such as salts and ethers of carboxymethylcellulose, dextrans and sugar solutions. Where the medicament is not easily wetted it may be desirable to incorporate a small proportion of a surface active agent into, and/or to use a solvent in the preparation of, the soft pellets or granules. In general we prefer not to use a binder, surface active agent or solvent (other than water) in the soft pellets or granules. When the medicament is hygroscopic a small proportion of water, which, if necessary, is added to the medicament in the vapour phase for pellets and in the liquid phase for granules is usually sufficient to act as binder. The moisture content of the material may be adjusted according to the physical properties of the particular material, for example, for disodium cromoglycate we prefer the soft pellets or granules to contain less than 15%, and preferably from 8 to 11% by weight of water. The size of the soft pellets or granules of the invention may be varied within the range 35 given above to suit the devices from which they are to be dispensed. For a given device there is an optimum pellet or granule size for optimum fluidisation of the soft pellets or granules and this may be readily determined by simple tests, e.g. by assessing the fluidisation of extremely strong pellets or granules within the device which it is intended to use. We have also found that optimum dispensing of the soft pellets or granules is related to the size of the hole in the container through which the pellets or granules are to issue. We prefer that the pellets or granules have a size of from one-twentieth to one-fifth of the diameter of the hole, which usually has a diameter of from 500 to 2,000 e.g. about 700 to 1,500 microns. As a general guide, we have found that satisfactory soft pellets or granules for use in insufflators of the type described in British Patent No. 1.122,284 (commercially available under the Registered Trade Mark 'Spinhaler') and powered by human inhalation have a mean size in the range of from 50 to 250 microns, preferably a mean size in the range 120 to 160 microns and most preferably a mean size of about 140 microns. The soft pellets or granules should be sufficiently coherent to be filled into containers, transported and stored, since appreciable break-up of the soft pellets or granules should not 50 occur under these conditions. From the above, it will be appreciated that soft pellets or granules having satisfactory properties may be obtained from a number of permutations of the size and coherence. B way of an example, we have found that for soft pellets or granules which are to be dispensed 55 from a gelatine capsule 6.4 mm in diameter and having two holes 0.8 mm in diameter in a shoulder thereof mounted in a device (commercially available under the Registered Trade Mark 'Spinhaler') according to British Patent No. 1,122,284 having a drawn wire shaft 2.03 mm diameter journalled in a hard nylon bearing tube 13 mm long and having an internal diameter of 2.08 mm at its inner end (i.e. that end housing the free end of the shaft) and of 2.44 mm at its other end, and wherein the capsule is rotated about its axis at a speed of about 1.800 rpm by an air stream having a flow rate of 60 litres per minute it is desirable that the pellets have a mean size of about 140 microns. It is especially preferred that the pellets or granules are made from disodium cromoglycate. The soft pellets or granules are preferably such that when put up in gelatine capsules 6.4

mm in diameter each containing 20 mg of the medicament as soft pellets or granules they

5

1 569 611

Total Transmitted Load Reduction It has also been found that with medicaments according to the invention which disperse satisfactorily the applied load transmitted to the load cell in the device described in

response of 1 g is registered by the load cell.

	(c) above does not increase steadily (see for example Figure 1). The back track of the curve, or the 'easing' of the load in grams, may be termed the 'Total Transmitted Load Reduction' of the material under test. Thus 'Total Transmitted Load Reduction' may be defined as the	
5	sum of the reductions in the transmitted load detected by the load cell while the load recorded as acting on the cell progresses from 0 to 1,000 gms. We have found that the most useful parameter in the definition of the pellets or granules according to the invention is the product of the 'Total Transmitted Load Reduction' and the 'Response Lag'.	5
10	The pellets and granules according to the invention have a lower loose bulk density than granules or pellets made by conventional techniques. Thus soft pellets and granules of disodium cromoglycate have a loose bulk density of less than 0.3 g per cc. preferably from 0.2 to 0.3 g per cc, and most preferably from 0.22 to 0.28 g per cc.	10
15	From another aspect the invention also provides a capsule, cartridge or like container containing soft pellets or granules of the invention, optionally in association with other pellets, granules or particles. We prefer the container to be loosely filled to less than about 80% by volume, preferably less than about 50% by volume, with the soft pellets or granules of the invention. The soft pellets or granules should of course not be compacted into the container. We prefer the container, e.g. capsule, to contain from 10 to 100 mg of the soft	15
20	pellets or granules. The container may conveniently be pierced (and overcapped, e.g. with a plastic overcap) during its manufacture and then used, after removal of the overcap, in an inhalation device which has no piercing mechanism.	20
25	Where it is desired to use the pellets or granules of the invention in association with other ingredients such as colourants, sweeteners or carriers such as lactose, these other ingredients may be applied, to or admixed with the pellets or granules using conventional techniques. We prefer the soft pellets or granules of the invention to contain medicament and water only and not to be mixed with any other ingredients.	25
30	The soft pellets or granules of the invention may be made by a number of methods. Thus according to the invention there is provided a method for the manufacture of soft pellets or granules according to the invention, which comprises subjecting particles of medicament (optionally in admixture with any other ingredient it is desired to incorporate into the pellets) which either are intrinsically, or have been rendered, self-agglomerative to a controlled agglomeration. This controlled agglomeration may be carried out by, (a) extruding the particles of medicament through an aperture,	30
35	 (b) controlled agglomeration in a fluidised bed, or (c) spray drying a solution or slurry of the medicament. In method (a) which is the preferred method, finely divided medicament, e.g. having a 	35
40	mean particle size in the range 0.01 to 10 microns may, if necessary, be subjected to an initial treatment to cause the powder particles to be self-agglomerative. Thus where the medicament is of a hygroscopic nature, the treatment may be carried out by exposing the powder particles to water.	40
45	When soft pellets are required the powder particles may be subjected to a humid atmosphere, for example at a temperature of from about 15° to 50°C. Whilst the amount of water required to achieve adequate self-agglomerative properties may vary from medicament to medicament, it will not usually be necessary to increase the water content of the powder beyond about 15% by weight, e.g. to from 5 to 10% when soft pellets are required. Where the medicament is non-hygroscopic, the necessary self-agglomerative properties may be imparted by the addition of a pharmaceutically acceptable binder, e.g.	45
50	one selected from those mentioned earlier, or by treating the powder with a liquid (under carefully controlled conditions), which may be evaporated to produce bridges of a solid residue binding the powder particles, or which causes adequate interparticle contact. It will be appreciated that the nature of the binder may affect the coherence of the resultant pellet or granule formed from treated medicament. A binder solution may, if desired, be used	50
55	with a hygroscopic medicament in order to improve the internal coherence of the resultant pellet or granule. After the particles have been rendered self-agglomerative, they are passed (optionally after being rolled in for example a drum or pan for a controlled time) through an aperture of approximately the size of the desired pellets, e.g. they are forced through the apertures of a vibrating sieve which is of similar mesh aperture to the desired final pellet or granule size. The product of this passage through an aperture are shaped	55
60	pre-pellets of the medicament. When soft granules are required the powder particles may be mixed with an excess of a suitable solvent, e.g. liquid water, and the moistened material passed through an aperture, e.g. a sieve such as a vibrating sieve, of approximately equal to or larger than the mesh size required in the final granules and then drying the resulting sieved material to the desired	60
	final solvent, e.g. water, content. The material may then be dry granulated to give the	

5	When it is desired to incorporate another ingredient, e.g. a binder, into the soft granules the other ingredient may conveniently either be mixed with the medicament before it is moistened or may be incorporated in the solvent used to moisten the medicament. The amount of water, or other solvent, used in the granulation can, under certain circumstances, be critical. Thus we have found that with di-sodium cromoglycate (DSCG) use of greater than about 25% by weight of water (measured on dry DSCG) causes the granules to be too strong and not to have satisfactory dispersion properties. We therefore prefer to use from about 12 to 25%, and preferably from 17 to 23% by weight of water in	5
10	the granulation of di-sodium cromoglycate. The drying is preferably effected in a preheated forced convection hot air oven. The temperature of drying is desirably from 60 to 100°C, and more especially from 80 to 90°C. The soft granules may also be made by controlled agglomeration of the medicament in a fluidised bed or by spray drying a solution or slurry of the medicament.	10
15	In process (b) the fine particles of medicament to be formed into pellets or granules may be suspended, together with any other ingredients it is desired to incorporate in the pellets or granules, in a gas stream in a fluidised bed apparatus. When a hygroscopic material is to be formed into pellets or granules the water content of the solid material may be adjusted by variation of the humidity of the gas stream passing through the fluidised bed for a time	15
20	and under conditions sufficient to produce pre-pellets or granules of the desired internal	20
25	In process (c) a solution or more preferably a sturry, of the medicament may be spray-dried to produce a soft granule. We prefer to use a sturry of discrete medicament particles of the desired fine particle size, the sturry also containing any other ingredients it is desired to incorporate in the granules. The liquid in the sturry is preferably a non-solvent or a poor solvent for the medicament so that no, or not many, medicament bridges are formed between the medicament particles during the spray drying. When a controlled amount of water is desired in the product a correspondingly greater amount of water may be included	25
30	in the liquid in the slurry. The extent of compaction of the treated powder during the controlled agglomeration will vary according to the method and powder used in the agglomeration. However, as a guide, we have found that suitable pre-pellets may be formed by process (a) from a powder of discillura cromoglycate containing from about 8 to 10% by weight of water, by forcing the	30
35	powder through a sieve having apertures of about 150 metron size. The pre-pellets produced by any of the above processes may, if desired or necessary be subjected to tumbling and agitation using conventional methods until the desired size, shape and coherence of the pellets are achieved. We prefer a proportion, e.g. a majority, of	35
40	spherical. Conveniently the tumbling and agitation are carried out in a pan or drum type of pelletising machine. The treatment of the pre-pellets in such a machine is carried out until the majority of pellets in the charge have a size within the desired range. The size of the pre-pellets used and the conditions used in their agitation and tumbling may be varied in known manner to achieve the desired final size of soft pellet. The time for which the pellets	40
45	are tumbled is, in certain circumstances, of importance to the production of viable soft pellets. The effect of the tumbling and agitation of the pellets is in general to strengthen them and increase their size slightly and to make them more nearly spherical in shape. As indicated above the final product which issues from the agitation or tumbling step will	45
50	have a range of sizes about the desired mean size. The product may be classified, e.g. sieved, to remove over and under sized material. The over and under sized materially may be broken down into very fine particles and recycled to the agglomeration stage if desired. The final soft pellets or granules may be put up in any suitable form of container such as a capsule or cartridge. Where it is desired to use the pellets or granules of the invention in association with other ingredients such as colourants, sweeteners or carriers such as lactose,	50
55	these other ingredients may be applied to or admixed with the penets of granules using conventional techniques. We prefer the soft pellets or granules of the invention to contain medicament and water only. The soft pellets or granules may also be used in admixture with up to 75% by weight of free particles of medicament having a diameter of from 0.01 to 10	55
60	According to our invention we also provide a method of dispersing a medicament, e.g. disodium cromoglycate, into an air stream wherein a pierced capsule containing a plurality of soft pellets or granules according to the invention is rotated and vibrated in an air stream. The rotation and vibration may conveniently be produced by any one of a number of devices, e.g. the device of British Patent Specification No. 1,122,284. Disodium	60
65	cromoglycate is known to be of use in the treatment of asthma and rhinitis. In this specification the term 'pellet' is used to denote an agglomerate which is held	65

together by interparticulate (e.g. Van der Waal's) forces and is typically made by a process involving water vapour. Pellèts are in general spherical in shape. The term 'granule' is used to denote an agglomerate which is held together by interparticle bridges. In the case of a soft granule these bridges are brittle. Granules can be of almost any shape. Granules are typically made by overwetting the medicament with solvent, e.g. water, and then removing some of the solvent. Pellets or granules comprising sodium cromoglycate and having a loose bulk density of less than 0.3 g per cc and particulate disodium cromglycate containing 12 to 25% by weight of water are described and claimed in our co-pending applications Nos. 5572/78 (Serial No. 10 1569612) and 5574/78. (Serial No. 1569613) The invention will now be illustrated by the following Examples in which all parts and percentages are by weight unless otherwise stated. Example 1 15 15 The moisture content of finely ground disodium cromoglycate having at least 98% thereof of particle size less than 10 microns and having a mass median diameter of from 1 to 3 microns was adjusted from an initial value of from 4 to 6% by weight to a value of about 9.5% by weight by exposure of the powder on a tray in an atmosphere of relative humidity 33% at 18 to 24°C. 20 20 After the desired moisture content had been achieved, the treated powder was (after an optional initial rolling in a drum pelletiser) tipped onto a 150 micron aperture stainless steel sieve screen mounted in a Russel vibratory sifter operating at a frequency of 1,000 cycles per second. The powder on the screen was forced through the sieve apertures using a stainless steel spatula pushed across the surface of the screen. The material issuing from the sifter as particles with a mean particle diameter of about 150 microns was fed directly to a drum pelletiser adapted to rotate about a horizontal axis. The drum of the pelletiser was approximately 0.3 m in internal diameter and 0.37 m long with one end closed and the other end provided with frusto conical shoulder leading to a 0.18 m orifice through which material could be charged to or removed from the drum. The interior of the drum was highly polished. Two kilograms of the material from the sifter were loaded into the drum which was then rotated at a peripheral speed of 0.38 m per second \pm 0.025 m per second for 15 minutes. At the end of this time the soft pellets had a mean particle diameter of 135 microns and not more than 10% by weight was retained on a 350 micron aperture sieve and not less than 90% by weight was retained on a 63 micron aperture sieve. The moisture content of the final soft pellets was in the range 8.5 to 10.5% by weight. It will be appreciated that those steps of the process carried out after adjustment of the moisture content of the initial powder should be carried out under conditions of controlled humidity so as not to alter the water content of the powder appreciably. The water used in the process should be sterile and the air used in the process should be Class 100 air. The soft pellets produced by the above procedure are approximately spherical, and have an open and loose structure and a fluffy surface when viewed under a microscope. Up to 90 mg, e.g. 40 to 60 mg, of the above soft pellets were placed in a gelatine capsule having two holes 0.8 mm in diameter pierced in the shoulder thereof which was mounted in a device as described in British Patent No. 1.122,284 having the detailed construction and dimensions referred to above. When air at a flow rate of 60 litres per minute was passed through this device, it was found that the charge in the capsule was consistently completely dispensed into the airstream and broken up to provide a cloud of very fine particles suitable for inhalation. By way of contrast, when the initial finely ground powder from which the pellets had 50 been prepared was tested under identical conditions, comparatively little of the powder was dispensed from test to test. Similar results were obtained when 1,3-bis(2-carboxychromon-7-yloxy)propan-2-ol disodium salt (6% water), isoprenaline sulphate and tetracycline were subjected to the procedure of the Example to obtain soft pellets. 55 Example 2 Using the device illustrated in Figure 2 and, pellets of di-sodium cromoglycate according to Example 1 a Response lag of greater than 0.4 cms, a Total Transmitted Load Reduction of greater than 900 gms and a dispersion of greater than 10% were obtained. 60 Example 3 1,000g of finely ground disodium cromoglycate of determined water content was placed

in the bowl of a planetary mixer. The calculated amount of water to bring the moisture content of the disodium cromoglycate to within the desired range was then added gradually, the sides of the mixer bowl being scraped regularly to ensure even moisture distribution.

The damp disodium cromoglycate was then passed through a vibrating sieve having a mesh size of 1,000 micron. The product was then dried in a preheated forced convection hot air oven at 85°C for 2 hours until the moisture content of the granules was in the range 5 to 8% by weight. The granules were then sieved through a 250 micron screen. The resulting granules were found to flow well and could be filled easily into gelatin capsules.	
Using the device illustrated in Figure 2, granules of disodium cromoglycate produced according to Example 3, and the Dispersion Test as previously described, dispersions of greater than 10% were obtained for granules made using from 10 to 25% by weight water at the granulation stage. These granules had response lags of greater than 0.3 cms and a Total Transmitted Load Reduction of greater than 100 gms.)
WHAT WE CLAIM 15:- 1. A medicament in pellet or granule form, wherein the pellet or granule is soft, is from 15 to 1,000 microns in diameter and comprises an agglomeration of individual medicament 15 particles at least 90% of which have a diameter of less than 10 microns, characterised in that	5
the pellets or granules have (i) a 'Total Transmitted Load Reduction' of greater than 100g, and/or (ii) a product of 'Total Transmitted Load Reduction' and 'Response Lag' of greater (iii) a product of 'Total Transmitted Load Reduction' and 'Response Lag' of greater 20 than 30 g/cms, and/or	Ó
(iii) a 'Response Lag' of at least 0.3 cms. 2. A medicament according to Claim 1, wherein the 'Total Transmitted Load Reduction' is greater than 400 g. 3. A medicament according to Claim 2, wherein the 'Total Transmitted Load 2	5
Reduction is greater than 600 g. 4. A medicament according to Claim 3, wherein the 'Total Transmitted Load	
Reduction' is greater than 1,000 g. 5. A medicament according to any one of the preceding claims, wherein the product of 'Total Transmitted Load Reduction' and 'Response Lag' is greater than 40 g/cms. 6. A medicament according to any one of the preceding claims, wherein the product of 'Total Transmitted Load Reduction' and 'Response Lag' is between 40 and 1,000 g/cms. 7. A medicament according to any one of the preceding claims, wherein the 'Response'	10
Lag' is at least 0.4 cms. 8. A medicament according to any one of the preceding claims, wherein the 'Response 1.2 ag' is between 0.4 and 0.8 cms.	35
Dispersion test as neremberore described, an unique impinger. medicament is found on the filter of the liquid impinger. 10. A medicament according to Claim 9, wherein an average total of at least 10% by	40
weight of medicament according to Claim 19, which impinger. weight of medicament is found on the filter of the liquid impinger. 12. A medicament according to any one of the preceding claims, wherein, in the Emptying test as hereinbefore described, an average of at least 50% by weight of the	45
45 Emptying test to material has emptied from each capsule. 13. A medicament according to Claim 12, wherein an average of at least 75% by weight of the material has emptied from each capsule. 14. A medicament according to Claim 13, wherein an average of at least 90% by weight to meach capsule.	
of the material has emptied from each capsairs, of the material has emptied from each capsairs. 50 15. A medicament according to any one of the preceding claims, wherein the pellet or	50
granules of mean size of from 50 to 250 microns. 17. A medicament according to Claim 16, wherein the mean size is from 120 to 160	55
18. A medicament according to Claim 17, wherein the mean size is 140 microns. 19. A medicament according to any one of the preceding claims, wherein at least 95% by weight of the medicament particles have a diameter of less than 10 microns. 19. Wherein at least 95% by weight of the	60
20. A medicament according to Claim 17, wherein at least 95% by weight of the medicament particles have a diameter of from 0.01 to 10 microns. 21. A medicament according to Claim 19, wherein at least 95% by weight of the medicament particles have a diameter of from 1 to 4 microns. 22. A medicament according to any one of the preceding claims, wherein the individual	
medicament particles are self-agglomerative. 65 23. A medicament according to any one of the preceding claims, wherein the	65

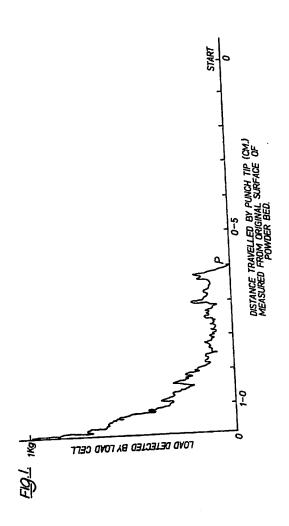
	medicament is hygroscopic. 24. A medicament according to any one of the preceding claims comprising an	
5	inhalation medicament for the treatment of allergic airway disease. 25. A medicament according to Claim 24, wherein the inhalation medicament comprises a pharmaceutically acceptable salt of 1,3-bis(2-carboxychromon - 5 - yloxy)propan-2-ol.	5
	26. A medicament according to Claim 25, wherein the inhalation medicament comprises disodium cromoglycate.	
10	27. A medicament according to Claim 26, wherein the inhalation medicament comprises disodium cromoglycate and isoprenaline.	10
10	28. A medicament according to Claim 26, comprising less than 15% by weight of water. 29. A medicament according to Claim 28, comprising from 5 to 10% by weight of water. 30. A medicament according to any one of the preceding claims, wherein the soft pellet	
15	is spherical. 31. A medicament according to any one of the preceding claims, in association with a	15
	colourant, sweetener or diluent. 32. A container containing a medicament according to any one of the preceding claims.	
20	 33. A container according to Claim 32 which is a capsule. 34. A container according to Claim 32 or 33 which is loosely filled to less than 80% by volume with the medicament in soft pellet or granule form. 35. A container according to Claim 34 which is loosely filled to less than 50% by volume 	2 0
	with the medicament in soft pellet or granule form. 36. A container according to any one of Claims 32 to 35 containing from 10 to 100 mg of	
25	the medicament in soft pellet or granule form. 37. A container according to any one of Claims 32 to 36 which is pierced.	25
	38. A method fo the manufacture of a medicament in pellet or granule form, wherein the pellet or granule is soft, is from 10 to 1,000 microns in diameter and comprises an the pellet or granule is soft, is from 10 to 1,000 microns in diameter and comprises an of the pellet or granule is soft, is from 10 to 1,000 microns in diameter and comprises an of the pellet or granule is soft, is from 10 to 1,000 microns in diameter and comprises an of the pellet or granule form.	
30	agglomeration of individual medicament particles at least 90% of which have a diameter of less than 10 microns, which comprises controlled agglomeration of medicament comprising individual medicament particles at least 90% of which have a diameter of less than 10 microns, characterised in that the pellets or granules have	30
	(i) a 'Total Transmitted Load Reduction' of greater than 100 g. and/or (ii) a product of 'Total Transmitted Load Reduction' and 'Response Lag' of greater	
35	than 30 g/cms, and/or (iii) a 'Response Lag' of at least 0.3 cms.	35
	39. A method according to Claim 38, wherein the controlled agglomeration comprises extruding the medicament comprising individual medicament particles through an aperture. 40. A method according to Claim 39, wherein the controlled agglomeration comprises forcing the medicament comprising individual medicament particles through a sieve of	40
40	similar mesh size to the desired final pellet size. 41. A method according to any one of Claims 38 to 40, wherein the medicament	40
	comprising individual medicament particles is subjected to an initial treatment to cause the particles to be self-agglomerative. 42. A method according to Claim 41, wherein the medicament is hygroscopic and the	
45	initial treatment comprises wetting the powder particles by exposing them to a numid	45
	43. A method according to Claim 42, wherein the particles are exposed to the humid atmosphere at a temperature of from 15 to 50°C.	
50	44. A method according to any one of Claims 38 to 41, wherein the medicament is	50
	45. A method according to Claim 38, wherein the controlled agglomeration is effected in a fluidised bed.	
55	46. A method according to Claim 38, wherein the controlled agglomeration comprises	55
	controlled agglomeration is subjected to tumbling and agitation. 48. A method according to Claim 47, wherein the tumbling and agitation are carried out	
60	in a pan or drum type of pelletising machine. 49 A method according to Claim 38 for the production of a soft granule which	60
	comprises mixing the individual medicament particles with an excess of a solvent, passing the moistened material through an aperture of equal to or larger than the size required in the final granules and then drying the resulting material to the desired final solvent content.	
65	50. A method according to Claim 49, wherein the solvent is water. 51. A method according to Claim 50, wherein the medicament is di-sodium cromogly-	65

	cate and the water content of the di-sodium cromoglycate before the drying is from 12 to	
5	25% by weight. 52. A method according to Claim 51, wherein the water content of the di-sodium cromoglycate before drying is from 17 to 23% by weight. 53. A method according to any one of Claims 49 to 52, wherein the temperature of drying is from 60 to 100°C.	5
10	to remove over and under sized material. 55. A method according to Claim 38 and substantially as hereinbefore described. 56. A method according to Claim 38 and substantially as hereinbefore described in any	10
10	one of the Examples. 57. A medicament in soft pellet or granule form when made by a process according to any one of Claims 38 to 56. 58. A method of dispersing a medicament into an air stream, wherein a pierced capsule containing a plurality of soft pellets or granules according to any one of Claims 1 to 31 or a container according to any one of Claims 32 to 37 is rotated and vibrated in an air stream.	15
20	C.B. CRAIG, Chartered Patent Agent, Agent for the Applicants, Fisons Limited.	2 0
25	Fison House, Princes Street, Ipswich, Suffolk, IP1 1QH.	25

Printed for Her Majesty's Stationery Office, by Croydon Printing Company Limited, Croydon, Surrey, 1980.
Published by The Patent Office, 25 Southampton Buildings, London, WC2A 1AY, from which copies may be obtained.

1569611 COMPLETE SPECIFICATION

This drawing is a reproduction of the Original on a reduced scale Sheet 1



COMPLETE SPECIFICATION

2 SHEETS

This drawing is a reproduction of the Original on a reduced scale .

Sheet 2

